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Complementary Modelling of Fluid Separation Processes

Despite that different fluid separations have much in common, a unified approach to their modelling is missing. This is mainly due to the diversity of operating, scale and boundary conditions as well as due to the significant modelling difficulties. A unified modelling approach is particularly difficult to formulate when a direct account of the process rates (transport and reaction kinetics) is essential, which is common in design and optimisation tasks. Therefore, we suggest an alternative way and present a novel modelling methodology which comprises different specific kinetics-based approaches and combine them in a complementary way. Such complementary modelling is a promising means to support the development of sustainable chemical engineering processes.



within the process

Fluid-dynamics approach

Idea: Process description by partial differential equations of fluid dynamics **Characteristics:**

Hydrodynamic analogy approache

Idea: Development of analogies between real complex fna mics and geometrically simpler flow patterns based on experimental observations

- Provides full information about the process (velocity, temperature
- and concentration field) in a purely theoretical way
- Difficult to apply for complex multiphase flow patterns **Results obtained:**
- Fim flows (cocurrent and countercurrent, laminar and turbulent, binary and multicomponent, one-, two- and three-phase, non-reactive) Liquid droplet and layer phenomena
- Monoliths





T. Atmakidis & E. Y. Kenig, 2007 Escape17, Bucharest, Romania

F. Atmakidis & E. Y. Kenig, 2007

Escape17, Bucharest, Romania

Fluid-dynamics approach Idea: Column sub-division onto segments (stages)

and their kinetics-based description

Characteristics:

- Suitable in design and optimisation tasks for many staged operations, including reactive and hybrid separations
- Weak point is that accuracy and predictivity strongly depend on the quality of model parameters

Results obtained:

Virtual experiments

Idea: Replacement of empirical

parameter estimation by modelbased simulations for different basic types of column internals

Characteristics:

- Extracts information from the investigation of small periodic representative elements of real internals (usually via CFD)
- Provides a link between FDA and RBA/HA
- Potentially, a way to virtual prototyping internals, however still in the early stage **Results obtained:**

Pressure drop in fixed beds

- and structured packings
- Residence time distribution in catalytic packings
 - Gas-liquid mass transfer coefficients in
 - catalytic packings
 - Liquid-solid mass transfer
 - coefficients in fixed
 - catalyst beds



Characteristics:

- Allows an extension of the application of partial differential equations to more complex objects and processes
 - Model parameters are directly
 - derived from the geometry of internals **Results obtained:**
 - Pertracton (liquid membrane extraction)
 - Microdistillation
 - Distillation in structured packed columns
 - Reactive stripping in packed columns and monoliths

methanol / acetonitrile / water (MEOH / ACN / WATER)





- Distillation and reactive distillation
- (Reactive) absorption and desorption
- Reactive Stripping
- Non-Reactive and reactive dividing wall columns
- Different Systems, units, internals
- Steady-state and dynamic simulations
- Optimisation studies
- Idea: Reaction kinetics measurements for CO₂ absorption into aqueous blends of alkanolamines prepared from renewable resources

Characteristics:

- Data are obtained in a stirred cell reactor with a plane, horizontal gas-liquid interface
- Easy-to-use experimental device operated batch-wise
- The method is based on a simple fall-in-pressure technique,

without measurements of concentrations

- **Results obtained:**
- Absorption of CO2 into aqueous solutions containing N,Ndiethylethanolamine (DEEA), N-ethylethanolamine (EEA) and ----their blends
- Reaction acceleration by piperazine (PIP)



P.D. Vaidya & E. Y. Kenig, 2007, Chem. Eng. Sci., 62, 7344-7350





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